

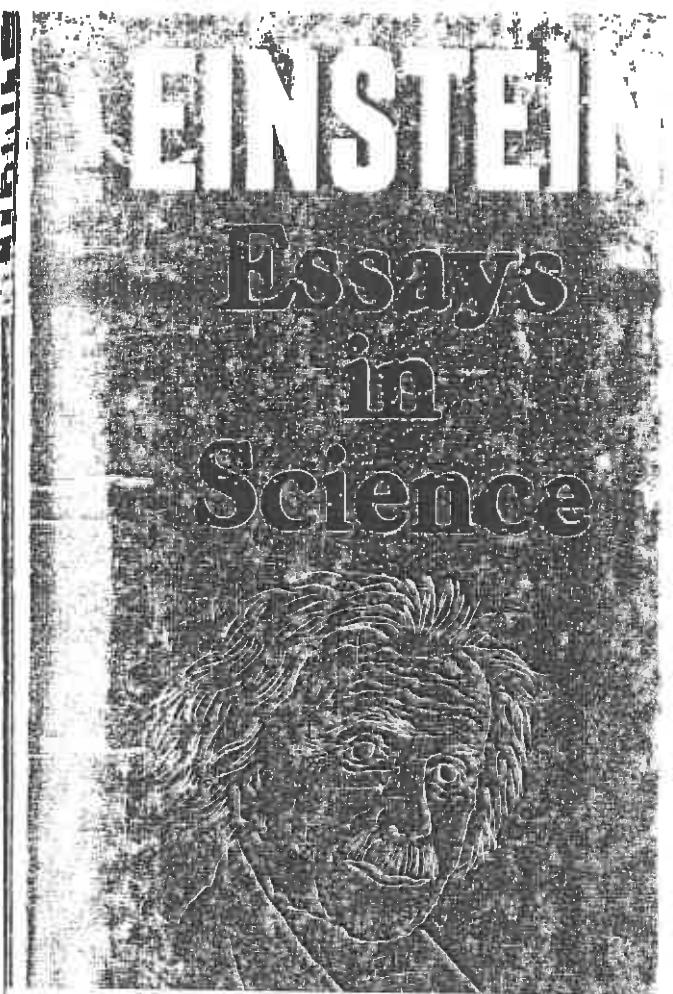
## Lecture 8

Check up dots from last time :

(1) Navier-Stokes Equations

(2) Bernoulli's equation  $\Rightarrow$

plus energy Bernoulli addition



physico-chemical factors (decomposition of the ground). We must concentrate our attention on the circumstances which affect the steepness with which the velocity falls at the wall.

In both cases the asymmetry in relation to the fall in velocity in question is indirectly due to the occurrence of a circular motion to which we will next direct our attention. I begin with a little experiment which anybody can easily repeat.

Imagine a flat-bottomed cup full of tea. At the bottom there are some tea leaves, which stay there because they are rather heavier than the liquid they have displaced. If the liquid is made to rotate by a spoon, the leaves will soon collect in the center of the bottom of the cup. The explanation of this phenomenon is as follows:—The rotation of the liquid causes a centrifugal force to act on it. This in itself would give rise to no change in the flow of the liquid if the latter rotated like a solid body. But in the neighborhood of the walls of the cup the liquid is restrained by friction, so that the angular velocity with which it circulates is less there than in other places near the center. In particular, the angular velocity of circulation, and therefore the centrifugal force, will be smaller near the bottom than higher up. The result of this will be a circular movement of the liquid of the type illustrated in fig. 1, which goes on increasing until, under the influence of ground friction, it becomes stationary. The tea leaves are swept into the center by the circular movement and act as proof of its existence.

## THE CAUSE OF THE FORMATION OF MEANDERS IN THE COURSES OF RIVERS AND OF THE SO-CALLED BEER'S LAW

IT IS common knowledge that streams tend to curve in serpentine shapes instead of following the line of the maximum declivity of the ground. It is also well known to geographers that the rivers of the northern hemisphere tend to erode chiefly on the right side. The rivers of the southern hemisphere behave in the opposite manner (Beer's law). Many attempts have been made to explain this phenomenon, and I am not sure whether anything I say in the following pages will be new to the expert; some of the relevant considerations are in any case known. Nevertheless, having found nobody who thoroughly understood the elementary principles involved, I think it is proper for me to give the following short qualitative exposition of them.

First of all, it is clear that the erosion must be stronger the greater the velocity of the current where it touches the bank in question, or the more steeply it falls to zero at any particular point of the confining wall. This is equally true under all circumstances, whether the erosion depends on mechanical or on

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## THE FORMATION OF MEANDERS

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The same sort of thing happens with a curving stream (fig. 2). At every section of its course, where it is bent, a centrifugal force operates in the direction of the outside of the curve (from A to B). This force is less near the bottom, where the speed of the current is reduced by friction, than higher above the bottom. This causes a circular movement of the kind illustrated in the diagram. Even where there is

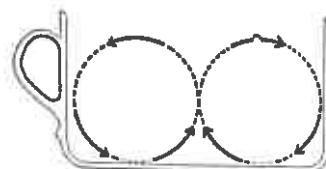


FIG. 1.

no bend in the river, a circular movement of the kind shown in fig. 2 will still take place, if only on a small scale and as a result of the earth's rotation. The latter produces a Coriolis-force, acting transversely to the direction of the current, whose right-hand horizontal component amounts to  $2 v \Omega \sin \phi$  per unit of mass of the liquid, where  $v$  is the velocity of the current,  $\Omega$  the speed of the earth's rotation, and  $\phi$  the geographical latitude. As ground friction causes a diminution of this force towards the bottom, this force also gives rise to a circular movement of the type indicated in fig. 2.

After this preliminary discussion we come back to

## Navier-Stokes equation

(3)

Substituting  $\sigma_{ij} = 2\mu e_{ij} + \lambda e_{mm} \delta_{ij}$   
into

$$\tilde{\epsilon}_{ij} = p_n \delta_{ij} + \sigma_{ij}$$

with Stokes assumption that  $\lambda + \frac{2}{3}\mu = 0$ ,

gives

$$(5-6) \quad \tilde{\epsilon}_{ij} = - \left\{ p_m + \frac{2}{3}\mu \nabla \cdot u \right\} \delta_{ij} + 2\mu e_{ij}$$

Substituting into

Cauchy  
eqn

$$\rho \frac{D u_i}{D t} = p_{,i} + \delta \tilde{\epsilon}_{ij} \frac{\partial u_j}{\partial x_i}$$

yields:

(5-7)  
Navier  
Stokes equation  
(isothermal-incompressible)

$$\rho \frac{D u_i}{D t} = - \nabla p_n + \rho g + \mu \nabla^2 u + \frac{1}{3} \mu \nabla \nabla \cdot u$$

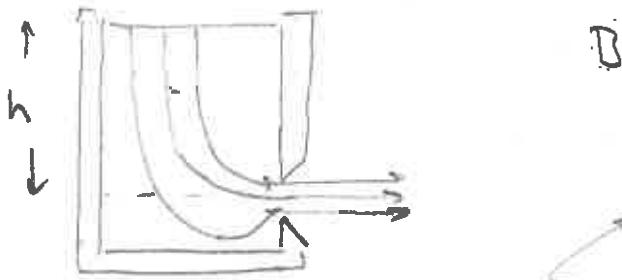
if flow is far from boundaries, viscous effect  $\rightarrow 0$

and

Euler  
equation  
(5-8)

$$\rho \frac{D u_i}{D t} = - \nabla p + \rho g$$

## (2.) Orifice in a Tank



$B = \text{constant along streamlines}$

$$= \frac{\rho^2}{2} + \frac{P}{\rho} + gz$$

$$= \frac{P_{\text{atm}}}{\rho} + gh \quad \text{at top}$$

$$= \frac{P_{\text{atm}}}{\rho} + \frac{u^2}{2} \quad \text{at jet}$$

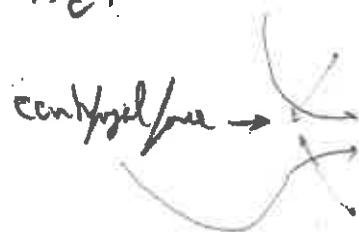
$$\therefore u = \sqrt{2gh}$$

$$\dot{m} = \text{mass flux at } = \rho A_c u$$

$$\boxed{\dot{m} = \rho A_c \sqrt{2gh}}$$

Note centrifugal force of curvy streamlines

$$\text{cav} \quad A_c^{\text{eff}} \approx 0.62 A_c$$



→  $\left[ \begin{array}{l} \text{Also note Bernoulli - total energy} \\ h + \frac{u^2}{2} + gz \end{array} \right] \quad \text{const along streamlines}$

Cavendish + conservation  $\rightarrow$  Newton's law  
 vorticity  
 Bernoulli  
 Energy "      Last time looked at  
 the way form of the  
 conservation of moment &  
 angular momentum.

## Lecture 8: Rotating frames

The final work we need to consider (for much of the earth, but not the moon) is the earth's rotation. Rotation gives rise to the coriolis force, which as anyone who has tried a rotating plate at a carnival knows, is try to force to be received up. Since our reference is the rotating surface of the earth, the coriolis force for oceanography and atmosphere dynamics is an important, in fact dominant, control.

The book does a good job of describing how the Navier-Stokes equation in a rotating frame changes from:

Navier-Stokes

(8-1)

$$\rho \frac{D\mathbf{u}}{Dt} = -\nabla p + \rho g + \mu \nabla^2 \mathbf{u}$$

where  $\mathbf{u}$  is the velocity of a material element in the fixed frame, to



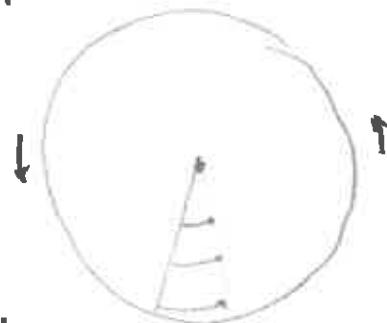
$$(8-2) \quad \text{(4.54 book)} \quad \rho \frac{D\mathbf{u}}{Dt} + 2\Omega \times \mathbf{u} - \frac{\Omega^2 R}{centrifugal} = -\nabla p + \rho g + \mu \nabla^2 \mathbf{u}$$

where  $\mathbf{u}$  is the velocity of a material element in the rotating frame. The material frame physics will be same in both frames, but acceleration terms

(2)

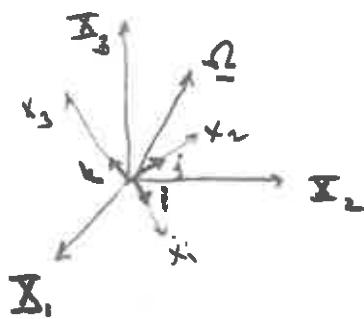
arise because  $\underline{v}$  is now measured in the rotating frame.

Consider a rotating platform



- As you walk out you must accelerate to "walk the straight line"
- in the rotating frame
- you acceleration is perceived as a centripetal force!
- We add this force to the Newton's law equation so it applies in the rotating frame

Consider a point  $\underline{P}$  in fixed + rotating frames

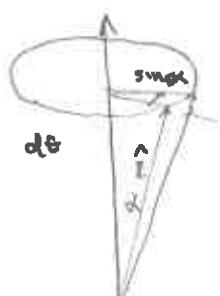


$$\underline{P}_R = P_{1R} \hat{i} + P_{2R} \hat{j} + P_{3R} \hat{k}$$

$$\left( \frac{d\underline{P}_R}{dt} \right)_F = \frac{d}{dt} (P_{1R} \hat{i} + P_{2R} \hat{j} + P_{3R} \hat{k})$$

$$= \hat{i} \frac{dP_1}{dt} + \hat{j} \frac{dP_2}{dt} + \hat{k} \frac{dP_3}{dt}$$

$$+ P_1 \frac{d\hat{i}}{dt} + P_2 \frac{d\hat{j}}{dt} + P_3 \frac{d\hat{k}}{dt}$$



$$\frac{d\hat{\underline{e}}}{dt} = \sin \alpha \frac{d\theta}{dt}$$

$$\underline{\Omega} \times \underline{i}$$

$$= \frac{d\underline{P}}{dt} + \underline{\Omega} \times \underline{P}$$

(2-3)

$$\boxed{\left( \frac{d\underline{P}}{dt} \right)_F = \left( \frac{d\underline{P}}{dt} \right)_R + \underline{\Omega} \times \underline{P}}$$

(3)

$$\text{Arrb to } \underline{\underline{P}} = \underline{\underline{r}}$$

$$\underline{\underline{u}}_F = \underline{\underline{u}}_R + \underline{\underline{\Omega}} \times \underline{\underline{r}}$$

$$\text{Arrb to } \underline{\underline{u}}_F$$

$$\left( \frac{d\underline{\underline{u}}_F}{dt} \right)_F = \left( \frac{d\underline{\underline{u}}_F}{dt} \right)_R + \underline{\underline{\Omega}} \times \underline{\underline{u}}_F$$

$$= \frac{d}{dt} (\underline{\underline{u}}_R + \underline{\underline{\Omega}} \times \underline{\underline{r}})_R + \underline{\underline{\Omega}} \times (\underline{\underline{u}}_R + \underline{\underline{\Omega}} \times \underline{\underline{r}})$$

$$\begin{aligned} \underline{\underline{A}} \times (\underline{\underline{B}} \times \underline{\underline{C}}) &= \\ &= (\underline{\underline{A}} \cdot \underline{\underline{C}}) \underline{\underline{B}} - (\underline{\underline{A}} \cdot \underline{\underline{B}}) \underline{\underline{C}} \end{aligned}$$

$$\begin{aligned} &= \left( \frac{d\underline{\underline{u}}_R}{dt} \right)_R + 2\underline{\underline{\Omega}} \times \underline{\underline{u}}_R + \underline{\underline{\Omega}} \times (\underline{\underline{\Omega}} \times \underline{\underline{r}}) \\ &\quad \downarrow \\ &= -(\underline{\underline{\Omega}} \cdot \underline{\underline{\Omega}}) \underline{\underline{R}} + (\underline{\underline{\Omega}} / \underline{\underline{R}}) \underline{\underline{\Omega}} \end{aligned}$$

$$\left( \frac{d\underline{\underline{u}}_F}{dt} \right)_F = \left( \frac{d\underline{\underline{u}}_R}{dt} \right)_R + 2\underline{\underline{\Omega}} \times \underline{\underline{u}}_R - \underline{\underline{\Omega}}^2 \underline{\underline{R}}$$

$$\underline{\underline{a}}_F = \underline{\underline{a}}_R + 2\underline{\underline{\Omega}} \times \underline{\underline{u}}_R - \underline{\underline{\Omega}}^2 \underline{\underline{R}}$$

Then the Navier-Stokes equation in the Fixed Frame

$$\left( \frac{D\underline{\underline{u}}}{Dt} \right)_F = -\frac{1}{\rho} \nabla p + \underline{\underline{g}} + \nu \nabla^2 \underline{\underline{u}}$$

becomes in rotating frame

effective gravity force  
"inertial force"

(2.4)

$$\left( \frac{D\underline{\underline{u}}}{Dt} \right)_R = -\frac{1}{\rho} \nabla p + \left( \underline{\underline{g}} + \underline{\underline{\Omega}}^2 \underline{\underline{R}} \right) + \nu \nabla^2 \underline{\underline{u}} - 2\underline{\underline{\Omega}} \times \underline{\underline{u}}$$

(4)

Coriolis acceleration is just that required for a projectile to follow the path we all know it should.

Consider standing on the pole of rotation and firing south.

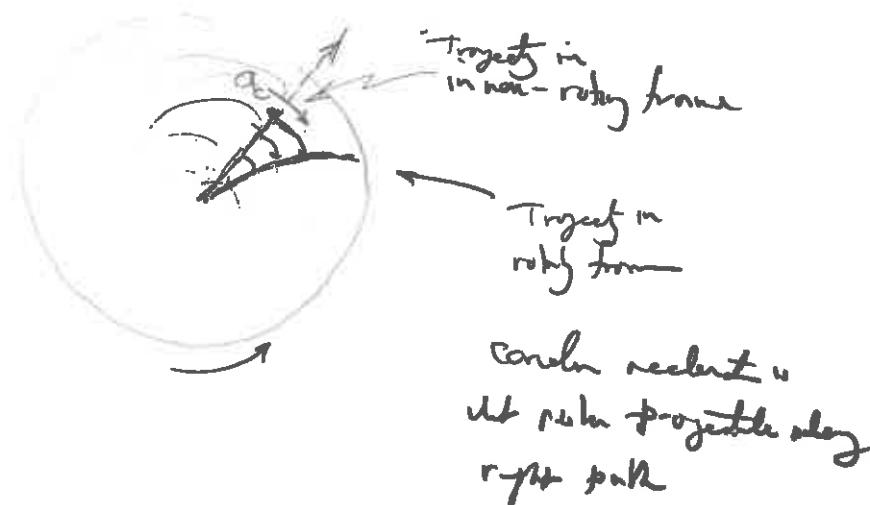
The projectile velocity  $u_p$  does not change.  $\therefore x_s = ut$ .

As projectile moves south rotation of earth  $\tau$ .  $a_c = 2\omega u_p$

$$\text{so } v_\theta = a_c t, \quad x_\theta = \int a_c dt = \frac{1}{2} a_c t^2 = \omega u_p t^2$$

$$\therefore \alpha = \frac{\Delta x_\theta}{\Delta x_s} = \frac{\omega t}{u_p t} = \text{just as if earth turned in } t.$$

$\therefore$  earth turns under projectile. "Acceleration" arises from fact  $u_p$  is not distance south. Acceleration defines the "fictitious" force need to "push" the projectile along its proper path.



# Vorticity

Incompressible  
Navier-Stokes

$$\frac{D\mathbf{u}}{Dt} = -\frac{1}{\rho} \nabla p + \mathbf{g} + \nu \nabla^2 \mathbf{u} - 2\mathbf{\Omega} \times \mathbf{u}$$

Euler

$$\frac{D\mathbf{u}}{Dt} = -\frac{1}{\rho} \nabla p + \mathbf{g} - 2\mathbf{\Omega} \times \mathbf{u}$$

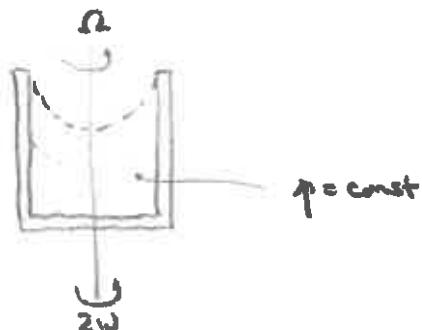
From basic  
physics

## Solid body rotation

}

$$F = \frac{\rho u_\theta^2}{r}$$

$$\frac{\partial p}{\partial r} = -\rho g \frac{\partial z}{\partial r}$$



$$\frac{\rho u_\theta^2}{r} - \rho g \frac{\partial z}{\partial r} = 0 \quad \text{force balance}$$

$$\text{Substitute } u_\theta = \frac{1}{2} \omega r$$

$$\int_{r_1}^{r_2} \frac{1}{4} \omega^2 r dr = \int_{z_1}^{z_2} g dz$$

$$\frac{1}{8} \frac{\omega^2}{g} (r_2^2 - r_1^2) = (z_2 - z_1)$$

(6)

Now from Euler equation

$$\frac{D\bar{u}}{Dt} = \frac{\partial \bar{u}}{\partial t} + \bar{u} \cdot \nabla \bar{u} = -\frac{1}{\rho} \nabla p + g$$

In polar coordinates (r, θ) with  $\bar{u}_r = 0$ ,  $\bar{u}_\theta = \frac{1}{2} \omega_0 r$

$$\begin{aligned} \cancel{\frac{\partial u_r}{\partial t} + u \cdot \nabla u_r} &= -\frac{1}{\rho} \frac{\partial p}{\partial r} + \nu \left( \nabla^2 u_r - \frac{u_r}{r^2} - \frac{2}{r^2} \frac{\partial u_\theta}{\partial \theta} \right) \\ \cancel{\frac{\partial u_\theta}{\partial t} + u \cdot \nabla u_\theta + u_r \frac{\partial u_\theta}{\partial r}} &= \frac{1}{\rho r} \frac{\partial p}{\partial \theta} + \nu \left( \nabla^2 u_\theta + \frac{\partial u_r}{r^2} + \frac{\partial u_\theta}{\partial \theta} - \frac{u_\theta}{r^2} \right) \\ \frac{\partial u_z}{\partial t} + (u \cdot \nabla) u_z &= -\frac{1}{\rho} \frac{\partial p}{\partial z} + \nu \nabla^2 u_z - g \end{aligned}$$

$$\text{From } p \text{ 73x } \sigma_{rz} = \mu \left[ \frac{1}{r} \frac{\partial u_r}{\partial \theta} + r \frac{\partial}{\partial r} \left( \frac{u_\theta}{r} \right) \right] = 0$$

and since by relation above  $u_\theta = \omega_0 r$ ,  $u_r = 0$ ,  $\sigma_{rz} = 0$

(7)

## Irrational Vortex

$$u_\theta = \frac{\Gamma}{2\pi r}$$

$$u_\theta = \frac{C}{r} \quad \text{, } u_r = 0$$

$$\omega = \nabla \times \underline{u}$$

$$\frac{\partial \sigma_{ij}}{\partial x_j} = -\mu (\underline{t} \times \omega)_i$$

$$= \frac{1}{r} \left( \frac{\partial}{\partial r} (r u_\theta) - \frac{\partial u_r}{\partial \theta} \right)$$

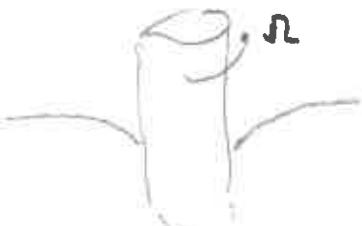
Since  $\omega = 0$  there is no viscous force. i.e. again inviscid Euler equation holds

$$-\frac{u_\theta^2}{r} = \frac{-1}{\rho} \frac{dp}{dr}$$

$$0 = -\frac{\partial p}{\partial z} - \rho g$$

so

$$dp = \frac{\rho \Gamma^2}{4\pi^2 r^3} dr - \rho g dz$$

Search  $\frac{1}{r}$  flow:

$$p_1 - p_2 = -\frac{\rho}{2} (u_{\theta 2}^2 - u_{\theta 1}^2) - \rho g (z_2 - z_1)$$

$$\frac{p_1}{\rho} + \frac{u_{\theta 1}^2}{2} + g z_1 = \frac{p_2}{\rho} + \frac{u_{\theta 2}^2}{2} + g z_2$$

Bernoulli equation valid between any two points (irrespective of just along streamline)

$$z_2 - z_1 = \frac{\Gamma}{2\pi^2 g} \left( \frac{1}{r_1^2} - \frac{1}{r_2^2} \right)$$

Toilet drain

## Kirchhoff's Circulation Theorem

$$\frac{D \Gamma}{Dt} = 0$$

Circulation is conserved  
in a material element!

$$\begin{aligned}\frac{D \Gamma}{Dt} &= \frac{D}{Dt} \int_C u_i dx_i \\ &= \int_C \frac{Du_i}{Dt} dx_i + \int_C u_i \frac{D}{Dt} dx_i\end{aligned}$$

Circulation around a  
material contour does  
not change

Momentum equation

$$\frac{Du_i}{Dt} = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + g_i + \frac{1}{\rho} \delta_{ij} \tau_{ij}$$

$$\int_C \frac{Du_i}{Dt} dx_i = - \int_C \frac{1}{\rho} \frac{\partial p}{\partial x_i} dx_i + \int_C g_i dx_i + \int_C \frac{1}{\rho} \delta_{ij} \tau_{ij} dx_i$$

$$\frac{D \Gamma}{Dt} = \int_C g_i dx_i - \int_C \frac{dp}{\rho} + \int_C \frac{1}{\rho} (\nabla \cdot \sigma) \cdot dx_i + \int_C u_i \frac{D}{Dt} dx_i$$

$$\vec{g} = -\nabla \Pi$$

$$\Pi_A - \Pi_B$$

$$\text{if } A = B \Rightarrow 0$$

barotropic

$$\tilde{\rho}^{-1} \approx \frac{dp}{dp}$$

$$P_B - P_A \Rightarrow 0$$

"  
of viscous

stress  
can be

neglected

$$d\vec{u} = \frac{D}{Dt} d\vec{x}$$

$$\int_C d(\frac{1}{2} \vec{u} \cdot \vec{u})$$

since  $u_i = \text{same}$   
at start + end  $\Rightarrow 0$

Create  
or destroy  
vortex

Non-conservative  
body forces

Non-barotropic  
pressure-p  
relation

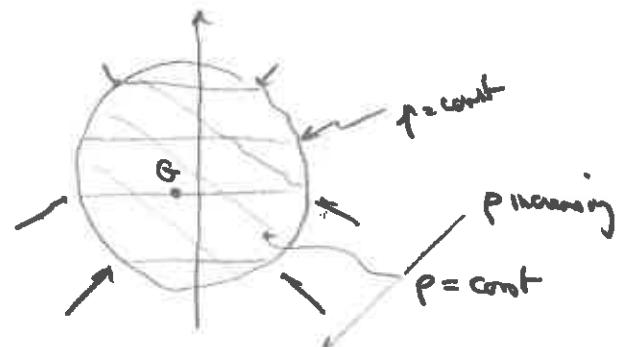
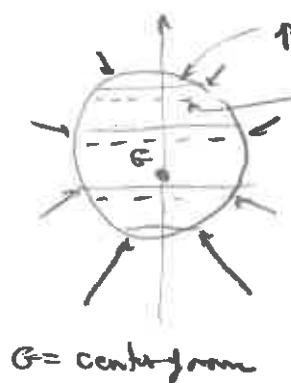
Viscous  
stress

## Implementation

- (1) Circulation is preserved
- (2) Viscous effect cause diffusion of vorticity in + out of circuit
- (3) Conservative body forces act through center of mass + do not produce vorticity
- (4) Barotropic flow - inviscid  
or  
 $\rho(p) \text{ of}$   
(perfect gas  $p/\rho = \text{const}$ )

lives of const  $P$   
parallel to living constant  $P$   
So the  $\nabla P$  acts at C of m

not barotropic = baroclinic



Produce corner vorticity

Geophysical flows which are dominated by baroclinicity are full of vorticity

Hattingy -  $\nabla_h P = 0$  necessary condition for viscous fluid

$\nabla_h P \neq 0$  generate vorticity

## Helmholtz Theorems

- (1) Vortex lines move with the fluid
- (2) Strength of vortex tube (its circulation) = const along length
- (3) Vortex tube cannot start or end  
(end at 'dry' or be closed loop - vortex ring)
- (4) strength of a vortex tube remains constant in time



vortex tube enclosing material particles

$S$  on boundary - circulation around edge of  $S = 0$

as tube moves  $S$  will move but  $\oint \mathbf{v} \cdot d\mathbf{l}$  with fluid  $\oint S = 0$

$\therefore$  no vortex out of tube anymore

$\therefore$  vortex confined in tube!

(11)

## Vertical equation

$$\frac{D\omega}{Dt} = (\underline{\omega} \cdot \nabla) \underline{u} + \omega \nabla^2 \underline{\omega}$$

$$= (\omega + z \Omega) \cdot \nabla u + \frac{1}{\rho^2} \nabla p \times \nabla p + \omega \nabla^2 \underline{\omega}$$

stretchy &  
tilting

bendlike  
curving  
vortex

diffuse

$$(\underline{\omega} \cdot \nabla) \underline{u} = \left[ \underline{\omega} \cdot \left( i_s \frac{\partial}{\partial s} + i_n \frac{\partial}{\partial n} + i_m \frac{\partial}{\partial m} \right) \right] \underline{u} = \omega \frac{\partial u}{\partial s}$$

along a vortex  
line  $s$

$\frac{\partial u}{\partial s}$  is stretchy along vortex line

$\frac{\partial}{\partial n}, \frac{\partial}{\partial m}$  represent turning or tilting of  
vortex line about  $m$  and  $n$  axes

$$\frac{Du}{Dt} = \omega \frac{\partial u}{\partial s}$$

$$\frac{Dw_s}{Dt} = \omega \frac{\partial u_s}{\partial s}$$

vertical change in  
stretch vortex line.  
stretch + angular speed!

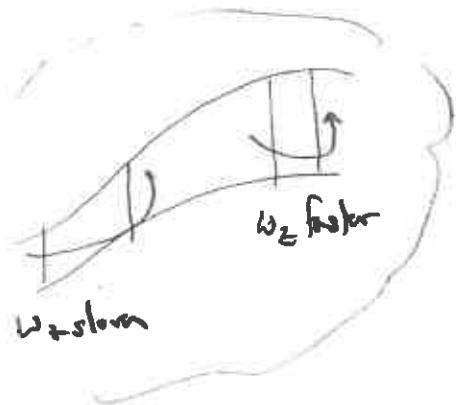
$$\frac{Dw_n}{Dt} = \omega \frac{\partial u_n}{\partial s}$$

tilting shift  
vortex into  
other component

$$\frac{Dw_m}{Dt} = \omega \frac{\partial u_m}{\partial s}$$

Stretch plays  
crucial role in  
dynamics of turbulent  
and geophysical flows

$$2(\underline{\Omega} \cdot \nabla) \underline{u}$$



if we orient z axis with  $\underline{\Omega}$

$$\frac{Dw}{Dt} = 2\Omega \frac{\partial u}{\partial t}$$

$$\frac{Dw_z}{Dt} = 2\Omega \frac{\partial w}{\partial t}$$

strictly no z  
increasing  $w_z$

Oceans vertical  
fluid lines constant  
"planetary vorticity"  
just trying to  
vertical fluid  
line is enough —  
vortex lines don't  
need to tilt

$$\frac{Dw_x}{Dt} = 2\Omega \frac{\partial u}{\partial z}$$

$$\frac{Dw_y}{Dt} = 2\Omega \frac{\partial v}{\partial z}$$

Tilt of  
vortex line  
change relative  
vortex in x and  
y directions

Kevin's circulation Theorem in rotating frame

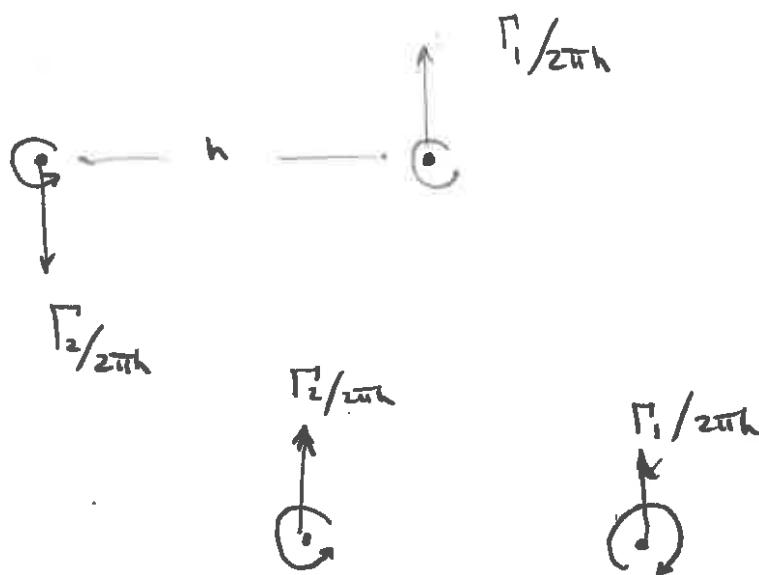
$$\frac{D\Gamma_a}{Dt} = 0$$

$$\Gamma_a = \int_A (w + 2\Omega) \cdot dA = \Gamma + 2 \underbrace{\int_A \Omega \cdot dA}_{\text{planetary vorticity}}$$

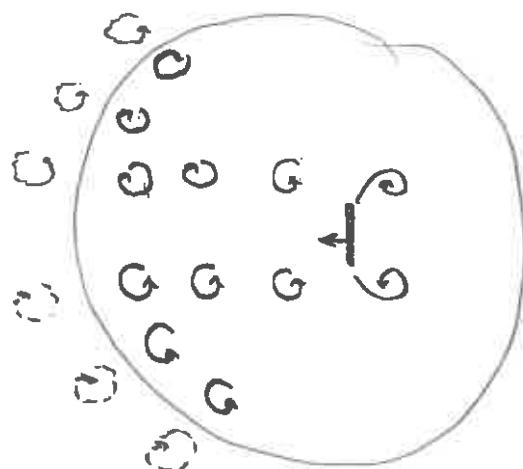
## Interaction of Vortices -

Vortices induce circulation at a distance ( $\frac{1}{r}$ ) and interact

Same sign  
rotate around  
each other



Opposite  
sign translate



opposite  
sign translate

## Smoke Ring + vortex sheet

2 rings equal size + same rotation

- front slows - sickle behind + ↑ in radius
- back speeds " of what + ↓ in radius
- from Pk - yoyo

Vortex sheet - discontinuity of velocity - aircraft wing

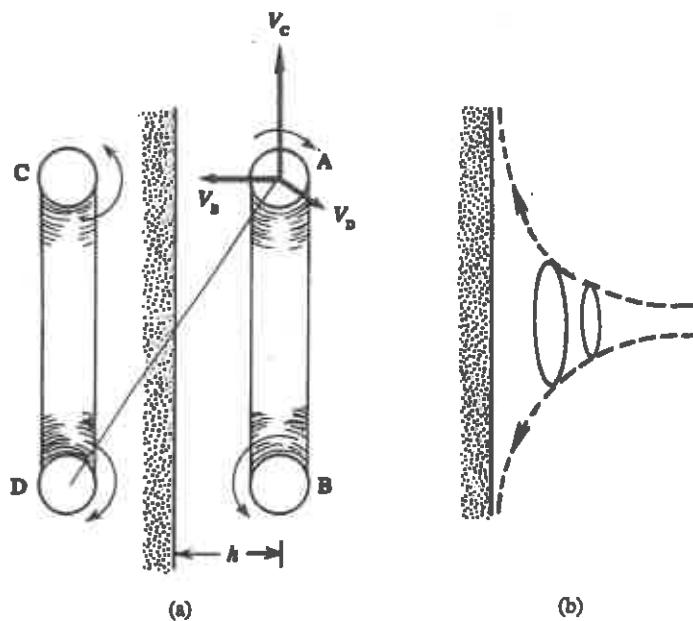


Figure 5.15 (a) Torus or doughnut-shaped vortex ring near a wall and its image. A section through the middle of the ring is shown. (b) Trajectory of vortex ring, showing that it widens while its translational velocity toward the wall decreases.

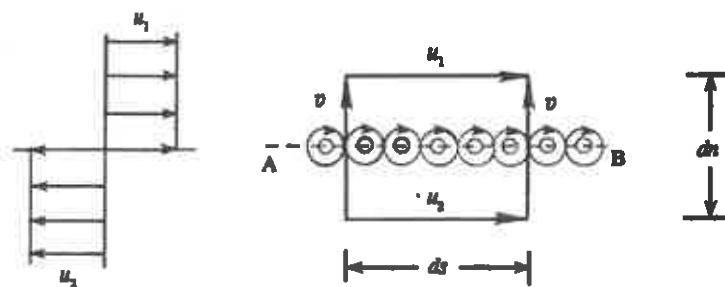


Figure 5.16 Vortex sheet.

## Chapter 6 - Irrotational flow

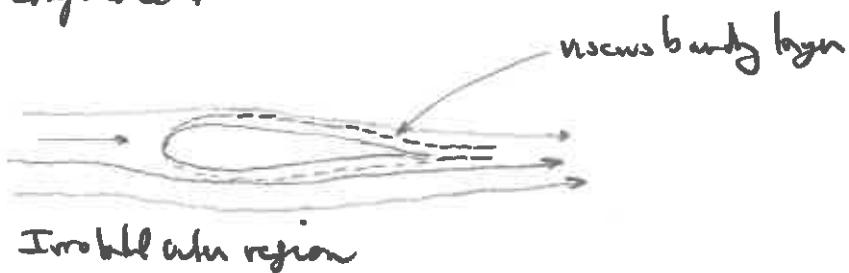
Irrotational flow stay irrotational

Rotated " " rotational

∴ Irrotational flow will become rotated at a body

÷ 2 regions - near body - "inner region"  
- far from body - "outer region"

Eddies can form!



can use complex variable & law of superposition to compute ideal streamlines + vorticity lines

Streamline velocity field

Add vortex circulation to flow around

a circular body

flow around sphere

vortex

$$U = \frac{\partial \psi}{\partial y} = \frac{\partial \phi}{\partial x}$$

$$W = U \left( z + \frac{a^2}{z} \right) + i \frac{\Gamma}{2\pi} \ln z/a$$

$$\omega = -\frac{\partial \psi}{\partial x} = \frac{\partial \phi}{\partial y}$$

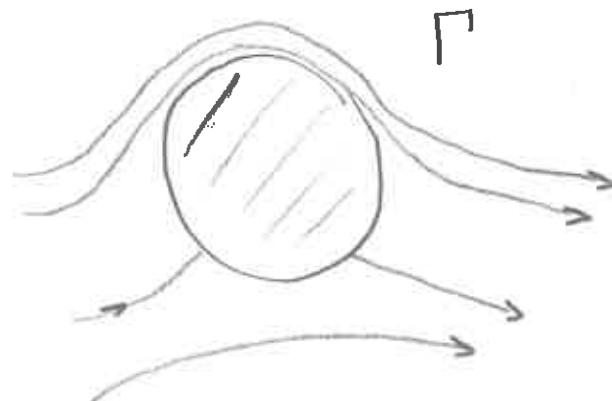
$$\psi = U \left( r - \frac{a^2}{r} \right) \sin \theta + \frac{\Gamma}{2\pi} \ln r/a$$

$$\frac{\partial \phi}{\partial x} = \frac{\partial \psi}{\partial y}$$

$$\frac{\partial \phi}{\partial y} = -\frac{\partial \psi}{\partial x}$$

} Cauchy-Riemann condition

$$z = x + iy = re^{i\theta}$$

U

With  
circulation  
added

App Bernoulli's principle to circulate option

Kutta - Zhukovsky

lift theorem

$$\boxed{L = \rho U \Gamma}$$

lift

Lift is proportional to circulation!

viscosity generates  $\Gamma$  but magnitude of  $\Gamma$  independent of visc + depends on  $U$ , shape + "attack" of the foil

Magnus effect  $\rightarrow$

for circular body - must rotate to get lift.

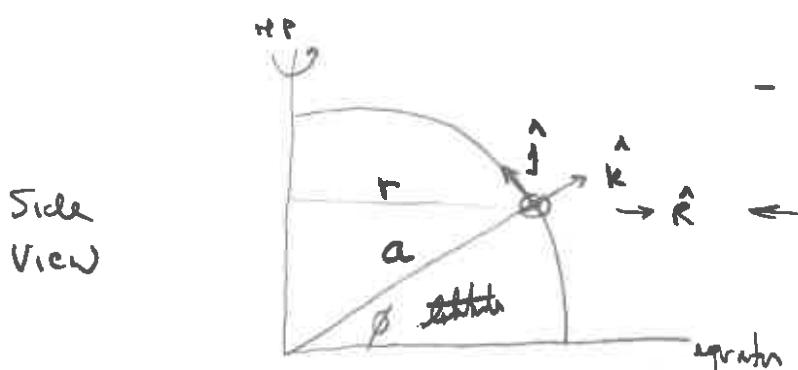
"golf ball" effect

$\rightarrow$

delay of separation of eddies also imp

March 8, 2016

Mark Wysotski



- Metrology convention

← unit vector in r direction

Side View

$$u \frac{D\hat{i}}{Dt}$$

$\hat{i} = \text{const} - \frac{\text{unit obj. v. time}}{\text{unit cent}}$

$$u \left( \frac{\partial \hat{i}}{\partial t} + u \cdot \frac{\partial \hat{i}}{\partial x} + \omega \frac{\partial \hat{i}}{\partial y} + \omega \frac{\partial \hat{i}}{\partial z} \right)$$

$\hat{i}$  point cent

$$\Delta \hat{i} = \hat{i} \Delta \lambda$$

$$u \frac{-\Delta \hat{i}}{\Delta x} = -r \Delta \lambda$$

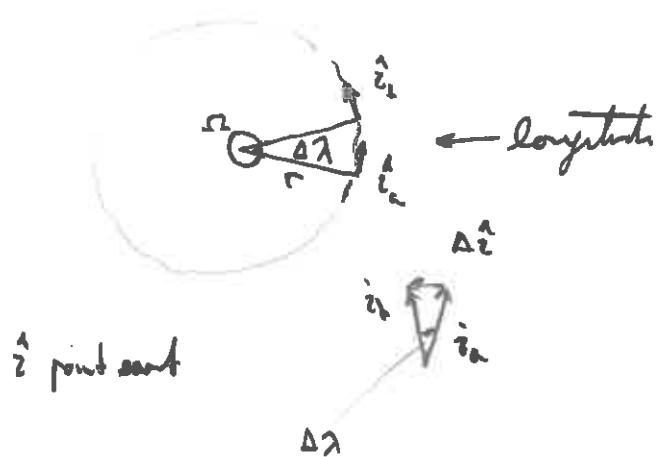
$$- u \frac{i \Delta \lambda}{r \Delta x} = - \frac{u}{r} \hat{R}$$

$$\frac{D\hat{i}}{Dt} = \frac{u^2}{a} \tan \phi \hat{j} - \frac{u^2}{a} \hat{k}$$

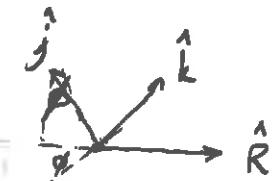
$$\hat{R} = (-\sin \phi \hat{j} + \cos \phi \hat{k})$$

$$\frac{\partial \hat{i}}{\partial x} = \frac{1}{r} u (\sin \phi \hat{j} - \cos \phi \hat{k})$$

$= a \cos \phi$



$$\sin \phi \hat{j} = -\hat{R}$$



$$\cos \phi (-\hat{k}) = -\hat{R}$$

$$\frac{\partial \hat{i}}{\partial x} = \frac{u}{a} \tan \phi \hat{j} - \frac{u}{a} \hat{k}$$

$$= \frac{\partial \hat{i}}{\partial x} = \frac{u}{a \cos \phi} (\sin \phi \hat{j} - \cos \phi \hat{k})$$

Typically on synoptic scale

48 hr - west of Earth

$$U = 10 \text{ m s}^{-1} \rightarrow \text{true}$$

$$a = 6.37 \times 10^6 \text{ m}$$

$$\phi = 45^\circ$$

$$\frac{u \frac{\partial i}{\partial t}}{a} = \frac{u}{a} \tan \phi j - \frac{u}{a} k$$
$$= 1.57 \times 10^{-6} \text{ m s}^{-2} = 1.5 \times 10^{-6} \text{ m s}^{-2}$$

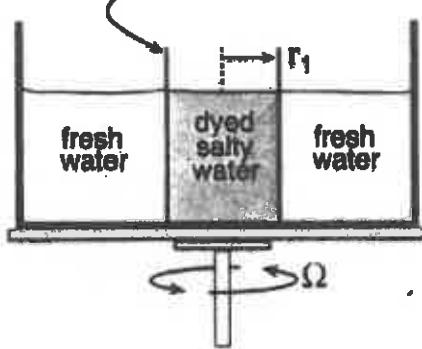
$$\approx \phi \text{ in mid latitudes}$$

cancel!

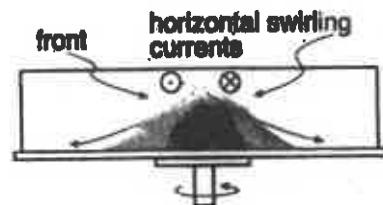
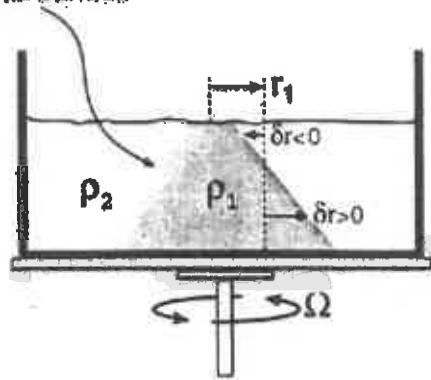
GCMs must take into account.

Synoptic flow - top border of Coriolis force

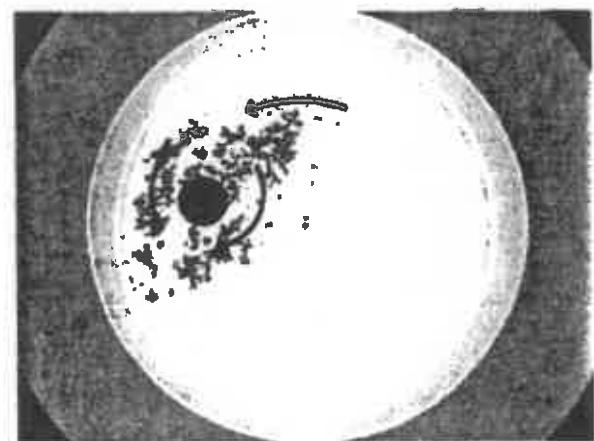
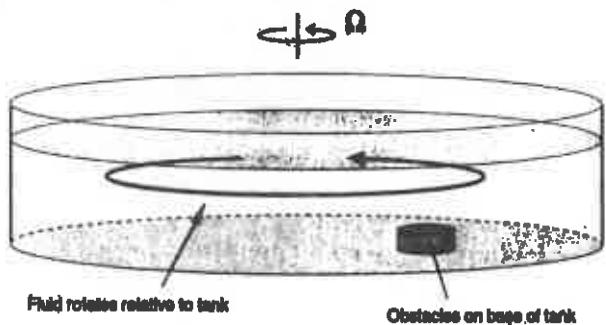
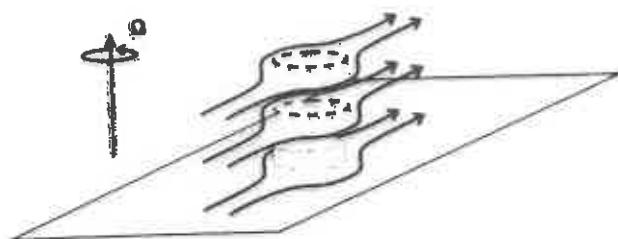
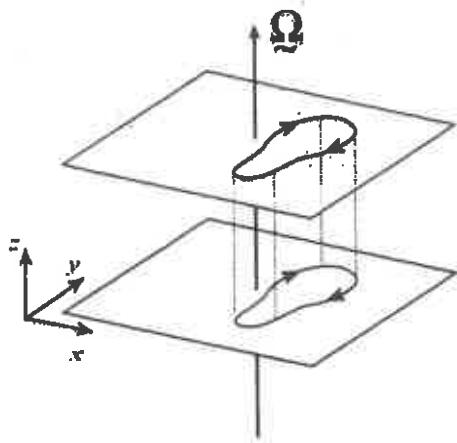
metal cylinder



frontal surface



salt water sinking under  
gravity and rotation



From man sheet + Durrant, 1998